

Chapter 2

2.1 40°API oil $\text{sp. gr.} = \frac{141.5}{131.5 + ^\circ\text{API}} = \frac{141.5}{131.5 + 40}$

$$\text{sp. gr.} = \frac{141.5}{171.5} = 0.825$$

2.2 $\text{sp. gr.} = 0.826$; $\rho = 1000(0.826) = 826 \text{ kg/m}^3$

$$\rho = 62.4(0.826) = 51.54 \text{ lbm/ft}^3$$

$$\text{sp. gr.} = \frac{141.5}{131.5 + ^\circ\text{API}} \quad 131.5 + ^\circ\text{API} = \frac{141.5}{0.826}$$

$$^\circ\text{API} = 171.3 - 131.5; \quad ^\circ\text{API} = 39.8^\circ\text{API} \approx 40^\circ\text{API}$$

2.3 $\text{sp. gr.} = \frac{141.5}{131.5 + ^\circ\text{API}} = \frac{141.5}{131.5 + 50} = 0.7796$ for a 50° oil

$$\text{sp. gr.} = \frac{141.5}{131.5 + ^\circ\text{API}} = \frac{141.5}{131.5 + 40} = 0.826$$
 for a 40° oil

$$0.825 - 0.7796 = 0.0455 \text{ density difference}$$

2.4 40°API oil $\text{sp. gr.} = \frac{141.5}{131.5 + ^\circ\text{API}} = \frac{141.5}{131.5 + 40} = 0.825$

$$\mu = 0.743 \text{ N}\cdot\text{s/m}^2 \quad \nu = \frac{\mu g_c}{\rho} = \frac{0.743}{0.825(1000)} = 9 \times 10^{-4}$$

Highly viscous; try

$$\nu = 0.2158 \times 10^{-6}(\text{SUS}) \quad \text{if } \text{SUS} > 215$$

$$\text{SUS} = \frac{9 \times 10^{-4}}{0.2158 \times 10^{-6}} = 4171 \text{ SUS}$$

2.5 Air at 27°C = 300 K has $\rho = 1.177 \text{ kg/m}^3$

CO₂ at 27°C = 300 K has $\rho = 1.797 \text{ kg/m}^3$

For a volume of 1.2 m³, the weight of air is

$$(1.177 \text{ kg/m}^3)(1.2 \text{ m}^3)(9.81 \text{ m/s}^2) = 13.86 \text{ N}$$

For CO₂

$$(1.797 \text{ kg/m}^3)(1.2 \text{ m}^3)(9.81 \text{ m/s}^2) = 21.15 \text{ N}$$

$$\text{Weight difference is } 21.15 - 13.86 = 7.29 \text{ N}$$

2.6 Castor Oil $\rho = 0.96(1000) \text{ kg/m}^3$

$$\frac{\text{buoyant force}}{\text{volume}} = \frac{mg_{\text{in air}} - mg_{\text{submerged}}}{Vg_c} = \frac{\rho g}{g_c}$$

$$\rho = \frac{10^{-7} \cdot 1}{(0.03)^3 \cdot 9.81} = \boxed{11\,330 \text{ kg/m}^3}$$

2.7 Buoyant force = $mg_{\text{in air}} - mg_{\text{submerged}} = mg - 0.8$ $g_c = 1$ in this system

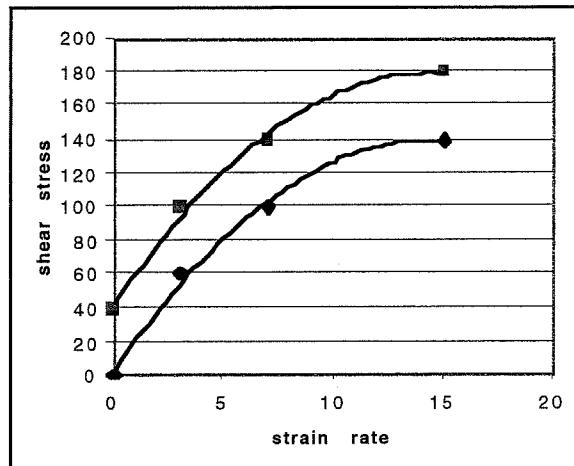
$$\frac{\text{buoyant force}}{\text{volume}} = \frac{mg - 0.8}{V} = \rho g \quad V = \frac{\pi D^2}{4} h = \frac{\pi}{4} (1/12)^2 (4/12) = 1.818 \times 10^{-3} \text{ ft}^3$$

$$mg = \rho_b V g = 8.5(1.94)(1.818 \times 10^{-3})(32.2) = 0.965 \text{ lbf}$$

$$\rho = \frac{mg - 0.8}{gV} = \frac{0.965 - 0.8}{32.2(1.818 \times 10^{-3})}$$

$$\boxed{\rho = 2.82 \text{ slug/ft}^3}$$

2.8 The topmost line is the given data, but to curve fit, we subtract 40 from all shear stress readings.



$$\tau = \tau_o + K \left(\frac{dV}{dy} \right)^n \quad \text{which becomes } \tau' = \tau - \tau_o = K \left(\frac{dV}{dy} \right)^n$$

Can be done instantly with spreadsheet; hand calculations:

dV/dy	ln(dV/dy)	τ	τ'	ln τ'	ln(τ') · ln(dV/dy)
0	—	40	0	—	—
3	1.099	100	60	4.094	4.499
7	1.946	140	100	4.605	8.961
15	2.708	180	140	4.942	13.38
Sum	5.753			13.64	26.84

$$m=3 \quad \text{Summation } (\ln(dV/dy))^2 = 12.33$$

$$b_1 = \frac{3(26.84) - 5.753(13.64)}{3(12.33) - 5.753^2} = 0.526$$

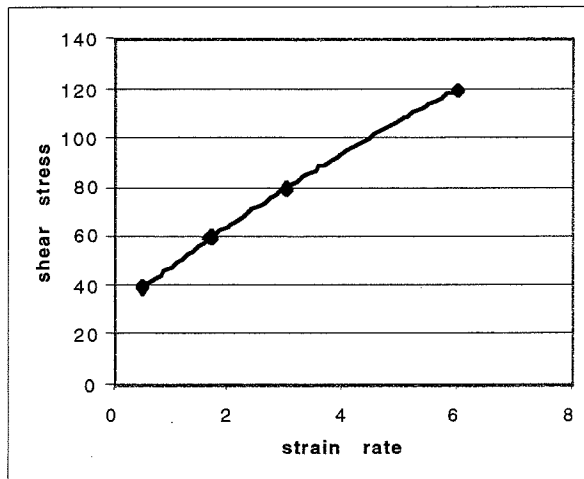
$$b_0 = \frac{13.64}{3} - 0.526 \frac{5.753}{3} = 3.537$$

$$K = \exp(b_0) = 34.37; \quad n = b_1 = 0.526$$

$$\tau = \tau_0 + K \left(\frac{dV}{dy} \right)^n = 40 + 34.37 \left(\frac{dV}{dy} \right)^{0.526}$$

where dV/dy is in rev/s and τ in g/cm^2 ; these are not standard units.

2.9 Cod liver oil; graph excludes the first data point.



$$\tau = K \left(\frac{dV}{dy} \right)^n$$

Can be done instantly with spreadsheet; hand calculations:

dV/dy	$\ln(dV/dy)$	τ	$\ln \tau$	$\ln(\tau) \cdot \ln(dV/dy)$
0.5	-0.6931	40	3.689	-2.557
1.7	0.5306	60	4.094	2.172
3	1.099	80	4.382	4.816
6	1.792	120	4.787	8.578
Sum	2.729		16.95	13.01

$$m=4 \quad \text{Summation } (\ln(dV/dy))^2 = 5.181$$

$$b_1 = \frac{4(13.01) - 2.729(16.95)}{4(5.181) - 2.729^2} = 0.4356$$

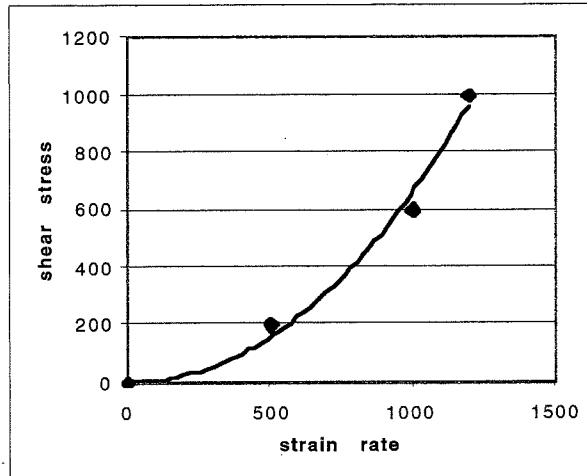
$$b_0 = \frac{16.95}{4} - 0.4356 \frac{2.729}{4} = 3.537$$

$$K = \exp(b_0) = 51.43; \quad n = b_1 = 0.4356$$

$$\tau = \tau_0 + K \left(\frac{dV}{dy} \right)^n = 51.43 \left(\frac{dV}{dy} \right)^{0.4356}$$

where dV/dy is in rev/s and τ in lbf/ft²; these are not standard units.

2.10 Vaseline



$$\tau = K \left(\frac{dV}{dy} \right)^n$$

Can be done instantly with spreadsheet; hand calculations:

dV/dy	ln(dV/dy)	τ	ln τ	ln(τ)·ln(dV/dy)
0	—	0	—	
500	6.215	200	5.298	32.93
1000	6.908	600	6.397	44.19
1200	7.090	1000	6.908	48.98
Sum	20.21		18.60	126.1